



# Electrochemical Performance of 1-Ethyl-3-Methylimidazolium Bis(Trifluoromethylsulfonyl)Imide Ionic Liquid as Electrolyte for Primary Mg-Air Batteries

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Ionic liquids are promising electrolytes for the primary Mg-air batteries. Three electrolytes, including pure 1-ethyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide ionic liquid, 50 mol.% butyl acetate and 50 mol.% water were studied. Attenuated total reflectance Fourier transform infrared spectroscopy, scanning electron microscopy and electrochemical impedance spectroscopy were used to examine discharge performance and the effects of butyl acetate and water additions. Galvanostatic measurements indicate that butyl acetate is an excellent additive, which can significantly improve the battery performance by reducing electrolyte impedance by increasing conductivity. However, while water also improved electrolyte discharge performance, it was consumed by the hydrogen evolution reaction over the 72 h discharge.

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Magnesium is a light, active metal with the standard potential of 2.37 V (vs. SHE) and potential capacity of  $-2,204$  mA·h/g, as excellent as lithium and aluminum.<sup>1-4</sup> Therefore, it can be used as an electrode material in batteries.<sup>5</sup> In recent years Mg-air batteries have received increasing attention due to the high energy density of up to 6,450 W·h/kg and stable performance.<sup>6,7</sup> Ionic liquids (IL) have been used in metal-air batteries due to their negligible vapor pressure, high thermal and electrochemical stability and non-flammability.<sup>8,9</sup>

Khoo et al.<sup>10-13</sup> have used the Grignard reagent ionic liquids in Mg-air batteries. Their studies showed that the Grignard reagent stabilized the interface between the Mg anode and the electrolyte and reduced magnesium self-corrosion. The addition of water improved the electrolyte conductivity and changed the anode surface microstructure. Thus, the discharge performance of the Mg-air battery was optimized. Kuboki et al.<sup>14</sup> reported the improved performance of the lithium-air batteries with a hydrophobic ionic liquid consisting of 1-alkyl-3-methyl imidazolium cations and perfluoroalkylsulfonyl imide anions. Also, 1-ethyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide demonstrated excellent electrolyte performance.<sup>14</sup>

Additionally, 1-butyl-1-methylpiperidinium bis(trifluoromethylsulfonyl)imide (PP<sub>14</sub>TFSI) ionic liquid was studied in dual-ion batteries,<sup>15</sup> Li-S cells<sup>16</sup> and in rechargeable batteries.<sup>17</sup> According to previous studies, water is a commonly used additive in ionic liquids. The possible roles of water have been identified. Water enhanced ion transport properties of IL by providing active protons to the cathodic oxygen reduction reaction. It also helped Mg<sup>2+</sup> ions to form an amorphous interface layer, which supports Mg dissolution.<sup>10,12,13,18</sup> This paper studied the electrochemical behavior of the primary Mg-air battery using the PP<sub>14</sub>TFSI as the electrolyte and further explored the effects of H<sub>2</sub>O and organic solvent butyl acetate (BA) additives. Previous studies found that H<sub>2</sub>O enhances the IL conductivity due to its high dielectric constant,<sup>19,20</sup> and butyl acetate is a widely used organic solvent to improve the mass transfer performance of the electrolyte.<sup>21</sup> The aim of this research is to analyze the feasibility of the additives to improve the performance of the PP<sub>14</sub>TFSI-based electrolytes in primary Mg-air batteries.

## Experimental

Pure magnesium (99.95%) has been used as the anode. The air electrode was made up of a waterproof layer, catalytic layer, and current collector. The waterproof layer was made of 40 wt% acetylene black as a conductive material and 60 wt% poly(tetrafluoroethylene) (PTFE) as a binding material. The catalytic layer was made of 37.5 wt% MnO<sub>2</sub>

and 25 wt% activated carbon as the catalyst and 37.5 wt% PTFE as a binding material. PP<sub>14</sub>TFSI was obtained from the Shanghai Cheng Jie Chemical Co. Ltd (Shanghai, China).

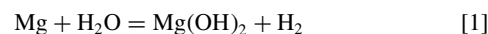
The electrochemical tests were performed using the CHI660C electrochemical workstation (CHI, USA). The open circuit potential (OCP) of working electrodes was measured using the 1 cm<sup>2</sup> exposed area. The electrochemical impedance spectroscopy (EIS) measurements were carried out at the OCP with a 5 mV sinusoidal modulation. The measurement frequency range was 10<sup>-2</sup>-10<sup>5</sup> Hz, starting with the higher frequency.

Galvanostatic discharge experiments were conducted using the CT2001A Landt discharge test system (Wuhan Lan Sheng Electronic Technology Co. Ltd, Wuhan, China). The sample surface after discharge was examined using scanning electron microscopy (SEM, JSM-5610LV). The electrolyte chemical composition was studied by the attenuated total reflectance Fourier transform infrared spectroscopy (ATR-FTIR). Additionally, conductivity and viscosity were investigated by the FE38 standard conductivity gauge (Mettler Toledo Instruments Co. Ltd, Switzerland) and DV-97+Pro viscosity meter (Shanghai Nirun Technology Company, China), respectively at 25°C, to verify the electrochemical results and examine the effects of BA and H<sub>2</sub>O.

## Results and Discussion

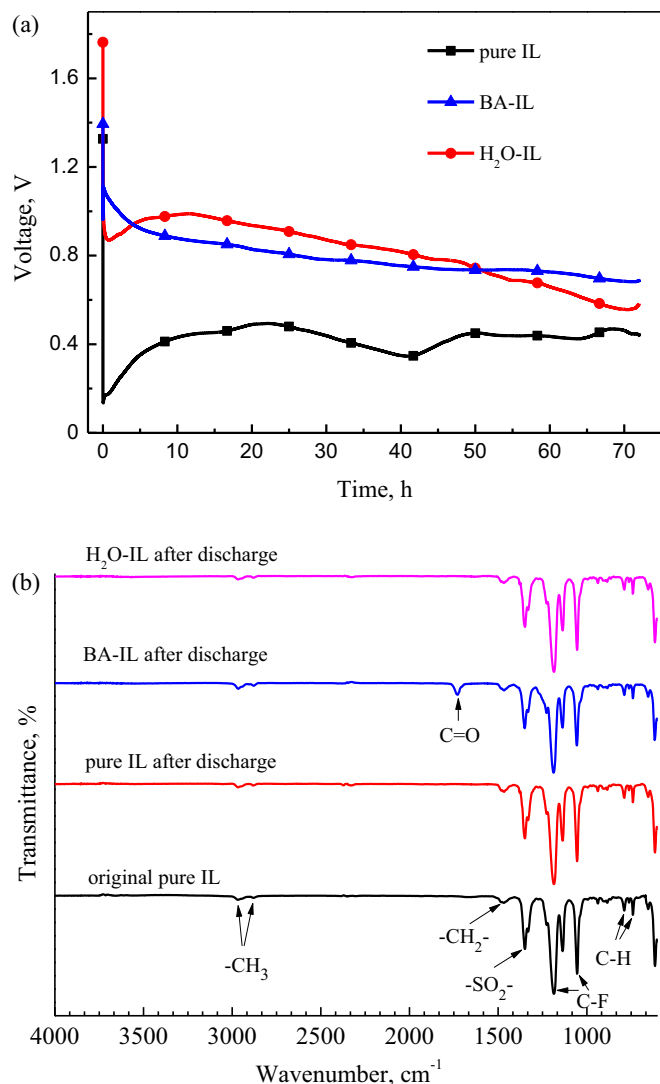
The galvanostatic discharge curves and the ATR-FTIR spectra of the electrolytes are shown in Fig. 1. The discharge current density was 0.1 mA/cm<sup>2</sup> in each case. As seen in Fig. 1a, the operating voltage rapidly decreased in the early discharge stage, caused by the internal resistance of the battery, and then reached an approximately constant value for the consequent 72 h. Compared with the IL mixture (H<sub>2</sub>O and BA added separately), the discharge performance of pure PP<sub>14</sub>TFSI exhibits instabilities, accompanied by lower voltage and more voltage fluctuations. Based on the discharge curves, H<sub>2</sub>O and BA additions resulted in higher and more stable voltage.

In the initial 10 h of discharge, the voltage of PP<sub>14</sub>TFSI with 50 mol.% H<sub>2</sub>O electrolyte gradually increased and declined thereafter. Normally, during the discharge process, the hydrogen evolution reaction occurs at the Mg anode:<sup>22,23</sup>



The consumption of H<sub>2</sub>O and the accumulation of Mg(OH)<sub>2</sub> may cause high electrical resistance of the electrolyte, resulting in deteriorated battery performance after 10 h of discharge. In this study, the action mechanisms of H<sub>2</sub>O on PP<sub>14</sub>TFSI were analyzed in detail.

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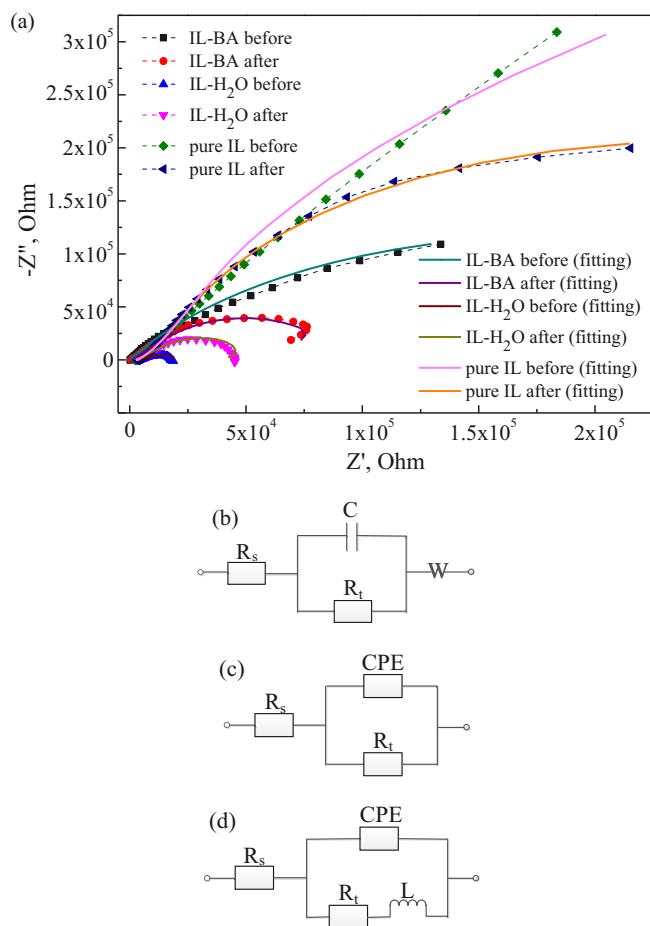


**Figure 1.** (a) Galvanostatic discharge curves and (b) ATR-FTIR spectra of electrolytes.

The discharge curve of the  $\text{PP}_{14}\text{TFSI}$  with 50 mol.% BA exhibits minimum fluctuations and BA has an outstanding performance over the 72 h galvanostatic discharge period, suggesting that BA is a stable additive for the  $\text{PP}_{14}\text{TFSI}$ .

As seen in Fig. 1b, the spectra from the original IL, IL after discharge and IL with added  $\text{H}_2\text{O}$  after discharge look quite similar. The chemical structure of  $\text{PP}_{14}\text{TFSI}$  didn't change after 72 h discharge. This illustrates that  $\text{PP}_{14}\text{TFSI}$  is a chemically stable electrolyte, which can withstand longer discharge. Lack of noticeable  $\text{H}_2\text{O}$  peak between  $3550\text{ cm}^{-1}$  and  $3230\text{ cm}^{-1}$  in the discharged  $\text{H}_2\text{O}$ -IL system implies that  $\text{H}_2\text{O}$  is involved in the hydrogen evolution reaction. The  $\text{PP}_{14}\text{TFSI}$  BA mixture results are similar to the original pure  $\text{PP}_{14}\text{TFSI}$ . According to the BA-IL system spectra, the peak at  $1728\text{ cm}^{-1}$  is assigned to the C=O bond of BA.<sup>24</sup> The ATR-FTIR results of the BS-IL system confirmed the effects of BA on the stability of  $\text{PP}_{14}\text{TFSI}$ .

The EIS plots of the three electrolytes before and after discharge are shown in Fig. 2a. BA and  $\text{H}_2\text{O}$  can effectively reduce the impedance and improve the mass transfer performance. The performance of  $\text{H}_2\text{O}$  is even more outstanding. Moreover, for the pure IL and 50 mol.% BA-IL systems, the resistance after discharge is obviously lower than before. This is perhaps caused by the collapse of the surface passivation layer on the Mg anode. However, the opposite result is observed in the 50 mol.%  $\text{H}_2\text{O}$ -IL. This is due to  $\text{H}_2\text{O}$  being consumed by the hydrogen



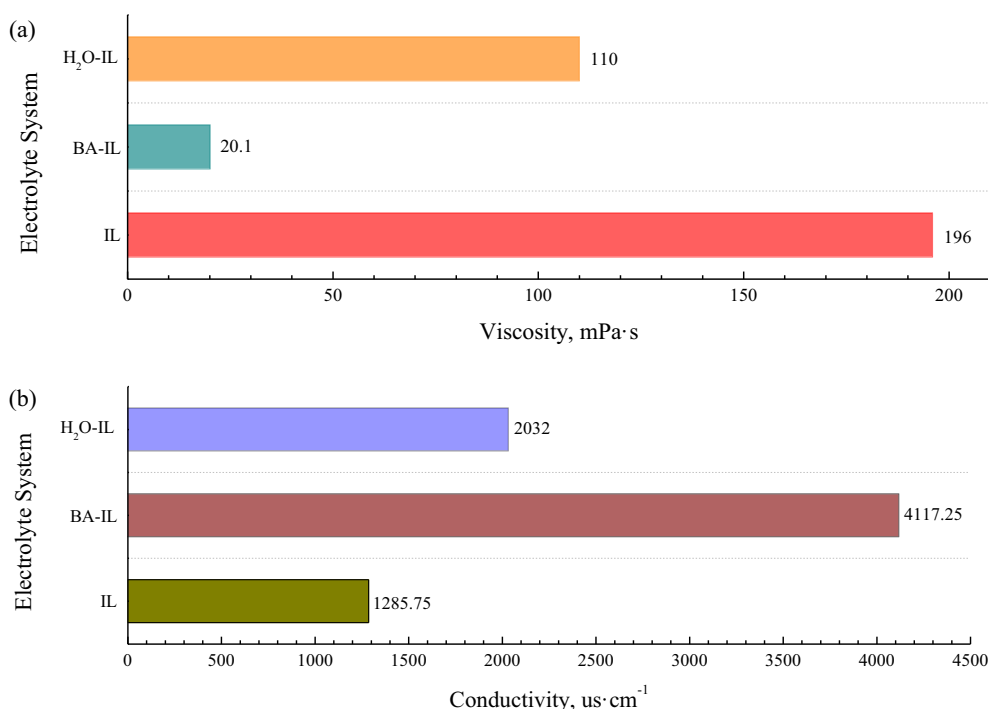
**Figure 2.** (a) EIS patterns of the three electrolytes before and after 72 h discharge; (b) Equivalent EIS circuits of pure IL before and after discharge; (c) Equivalent EIS circuits of BA-IL and  $\text{H}_2\text{O}$ -IL before discharge; (d) Equivalent EIS circuits of BA-IL and  $\text{H}_2\text{O}$ -IL after discharge.

evolution reaction during the discharge process. The capacitive loops in each electrolyte system are related to the interfacial electrochemical reactions and the interface charge transfer, although the capacitive loops of pure IL and BA-IL systems before discharge are incomplete. Noteworthy, sloped lines, which represent the diffusion process in the electrolyte, are obtained in the IL systems, indicating the difficulty of charge transfer in pure  $\text{PP}_{14}\text{TFSI}$ .<sup>25</sup>

To further investigate the impedance of the three systems, several equivalent circuits were constructed in Figs. 2b–2d. In Figs. 2b–2d,  $R_s$  represents the solution resistance,  $R_t$  and CPE or C are the charge transfer resistance and double layer capacitance of the Mg surface, and L is the inductance. W is the Warburg impedance, describing the diffusion process in pure IL electrolyte. The fitted values of the equivalent elements are listed in Table I. Low  $X^2$  variance values reflect good fits of electrolytes impedance.

In Fig. 2b, the W element explains electric charge transfer difficulty in pure IL due to the enormous  $\text{PP}_{14}\text{TFSI}$  ionic group size and high viscosity, causing large mechanical drag force. The lack of W element in Figs. 2c and 2d indicates that BA and  $\text{H}_2\text{O}$  make charge transfer more effective. The effects of BA and  $\text{H}_2\text{O}$  on viscosity are shown in Fig. 3a. Obviously, the viscosity decreased significantly with added BA, owing to its small molecular size and excellent miscibility with  $\text{PP}_{14}\text{TFSI}$ . The impact of  $\text{H}_2\text{O}$  on viscosity is relatively low but still plays its role on the charge transfer.

In Table I, the  $R_s$  parameter values suggest that BA can significantly reduce the solution resistance, but  $\text{H}_2\text{O}$  has no effect at all. Accordingly, the conductivity of the three electrolytes is shown in Fig. 3b, the



**Figure 3.** (a) Viscosity of the three electrolytes; (b) Conductivity of the three electrolyte.

results are in correspondence with  $R_s$ . Obviously, the consequences contradict to the coulomb force law:

$$F = \frac{Q_1 Q_2}{4\pi\epsilon_0\epsilon_r r^2} \quad [2]$$

where  $F$  is the electrostatic force,  $Q_1$  and  $Q_2$  are point electric charges,  $\epsilon_0$  is vacuum permittivity,  $\epsilon_r$  is relative permittivity of the medium, and  $r$  is the distance between the two charges. The electrostatic force inhibits the electrolytic dissociation, and with high force, most of the ionic species exist as ion pairs. Ion pairs contribute neither ionic strength nor ionic conductivity to the solution.<sup>26</sup> According to the coulomb force law, the electrostatic force of attraction between two ions with the opposite charge decreases with the increase of  $\epsilon_r$ . The permittivity of BA and H<sub>2</sub>O is 5.07 and 78.36 F/m respectively,<sup>27</sup> however, H<sub>2</sub>O lost its proper role due to low solubility in IL. Thus it can be seen that both favorable miscibility and permittivity are necessary.

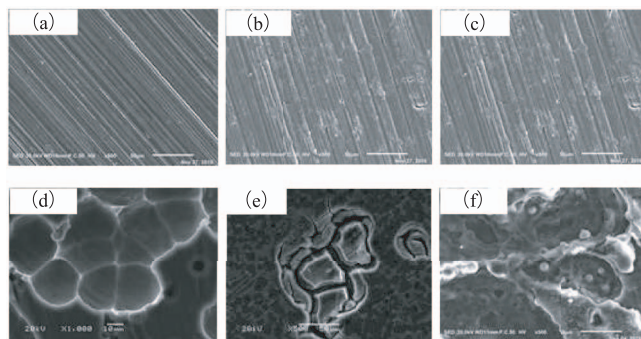
As for the interface processes, double layer capacitance  $C$  in pure IL in Fig. 2b is replaced by the CPE element in Figs. 2c and 2d, and the  $n$  parameter for the CPE is between 0.529 and 0.713 in Table I. This illustrates that H<sub>2</sub>O and BA reduce the Mg anode interface stability.

Moreover, it is noteworthy that H<sub>2</sub>O decreases the charge transfer resistance by one order of magnitude, which can be observed by

comparing the  $R_t$  values in each system, revealing that H<sub>2</sub>O plays an essential role in the interface process of charge transfer. For the H<sub>2</sub>O-IL system, H<sub>2</sub>O improved the chemical properties of the interface between Mg anode and an organic electrolyte solution and then promoted the electrochemical process of charge transfer by extracting it from the anode and transferring it to the electrolyte. The difficult degree of the charge transfer also can be reflected by the SEM images of the Mg anode surfaces before and after 72 h discharge in pure IL, 50 mol.% BA-IL and 50 mol.% H<sub>2</sub>O-IL electrolytes, as shown in Fig. 4. In contrast, more pronounced discharge morphology could be seen on the Mg surface of H<sub>2</sub>O-IL in Fig. 4f, which corroborated the positive effect of H<sub>2</sub>O on the electrode/electrolyte interface, accompanying inevitable self-corrosion. The round-like bulges in Fig. 4f suggest that there was gas generated at the interface during the discharge process, which further proves hydrogen evolution on the Mg surface in the H<sub>2</sub>O-IL system. Beyond that, the wide and deep cracks on the electrode locally of BA-IL in Fig. 4e and the morphology in Fig. 4f agree with the inductance results in Fig. 2d, representing intergranular corrosion of the Mg anode.

**Table I.** EIS elements values simulated using the corresponding equivalent circuits.

Electrolyte	Pure IL		BA-IL		H <sub>2</sub> O-IL	
	Before	After	Before	After	Before	After
$R_s$ ( $\times 10^3, \Omega\cdot\text{cm}^2$ )	2.699	3.102	0.27	0.809	3.552	3.389
CPE ( $\times 10^{-5}, \text{F}\cdot\text{cm}^{-2}$ )	-	-	3.048	3.515	4.087	4.473
$n$ ( $0 < n < 1$ )	-	-	0.713	0.621	0.529	0.568
$R_t$ ( $\times 10^5, \Omega\cdot\text{cm}$ )	6.109	2.84	3.738	1.231	0.173	0.479
$L$ ( $\times 10^5, \text{H}\cdot\text{cm}^2$ )	-	-	-	5.332	-	2.049
$C$ ( $\times 10^{-5}, \text{F}\cdot\text{cm}^{-2}$ )	4.576	5.315	-	-	-	-
$W$ ( $\times 10^{-5}, \Omega\cdot\text{cm}^2$ )	3.652	4.537	-	-	-	-
Variance, $X^2$ ( $\times 10^{-3}$ )	2.091	7.224	6.351	5.848	7.843	5.842



**Figure 4.** SEM micrographs of the Mg-anode in different electrolytes before and after 72 h discharge: (a) pure IL before, (b) BA-IL before, (c) H<sub>2</sub>O-IL before, (d) pure IL after, (e) BA-IL after, (f) H<sub>2</sub>O-IL after.

Further work is underway to research the mechanism and optimal dosage of additives. Obviously, the battery structure is also crucial and is currently under investigation.

### Conclusions

Electrochemical performance of the PP<sub>14</sub>TFSI ionic liquid, BA-IL and H<sub>2</sub>O-IL mixtures as an electrolyte for the Mg-air battery was investigated. The PP<sub>14</sub>TFSI ionic liquid can sustain 72 h discharge. BA increased the discharge voltage and made it more stable. Meanwhile, H<sub>2</sub>O has a similar action, but the effect was degraded by the hydrogen evolution reaction. Based on the EIS, equivalent circuits, viscosity, conductivity and SEM results, both BA and H<sub>2</sub>O have excellent performance in terms of improving electrolyte charge diffusion by decreasing electrolyte viscosity. Furthermore, BA reduces electrolyte impedance by increasing conductivity, and H<sub>2</sub>O improves conductivity at the interface between the anode and the electrolyte.

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